Appln. No.: 09/832,378 JMYT-224US1

Amendment Dated May 17, 2004

Reply to Office Action of February 17, 2004

<u>Amendments t the Claims:</u> This listing of claims will replace all prior versions, and listings, of claims in the application

Listing of Claims:

1. (Currently Amended) A process for the catalytic generation of hydrogen by the self-sustaining combination of partial oxidation and steam-reforming of a hydrocarbon comprising contacting a mixture of the hydrocarbon and an oxygen-containing gas and steam with a catalyst comprising rhodium dispersed on a refractory oxide support material which comprises as cations cerium and zirconium, wherein the weight ratio of cerium to zirconium in the support material is from 50:50 to 99.5:0.5.

- 2. (Previously Presented) A process according to claim 1 wherein the stream is combined with the hydrocarbon and the oxygen-containing gas to form the mixture after the self-sustaining partial oxidation of the hydrocarbon has commenced.
- 3. (Previously Presented) A process according to claim 1 wherein the hydrocarbon is a straight chain hydrocarbon or a branch chain hydrocarbon.
- 4. (Original) A process according to claim 3 wherein the hydrocarbon contains 1 to 15 carbon atoms.
- 5. (Original) A process according to claim 4 wherein the hydrocarbon contains 1 to 7 carbon atoms.
- 6. (Previously Presented) A process according to claim 1 wherein the hydrocarbon is selected from methane, propane, butane, hexane, heptane, normal-octane, iso-octane, naphthas, liquified petroleum gas, reformulated petrol and diesel-type fuels.
- 7. (Previously Presented) A process according to claim 1 wherein the oxygen-containing gas is air.
- 8. (Previously Presented) A process according to claim 1 wherein rhodium comprises 0.1 weight *per cent* to 5 weight *per cent* of the total weight of the supported catalyst.
- 9. (Original) A process according to claim 8 wherein rhodium comprises 0.2 weight *per cent* to 2.5 weight *per cent* of the total weight of the supported catalyst.

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10. (Previously Presented) A process according to claim 1 wherein the refractory oxide support material is a mixture of ceria and zirconia.

- 11. (Canceled)
- 12. (Canceled)
- 13. (Previously Presented) A process according to claim 1 wherein the catalyst is pre-heated to a temperature at which self-sustaining partial oxidation of the hydrocarbon commences.
- 14. (Original) A process according to claim 13 wherein the catalyst is pre-heated by direct heating to a temperature at which self-sustaining partial oxidation of the hydrocarbon commences.
- 15. (Original) A process according to claim 13 wherein the catalyst is pre-heated by catalytic heating to a temperature at which self-sustaining partial oxidation of the hydrocarbon commences.
- 16. (Currently Amended) A process according to claim 15 wherein the catalyst is pre-heated by feeding to the catalyst an oxygen-containing gas and an initiating compound which is more easily-oxidisable oxidizable than the hydrocarbon which is to be partially-oxidised oxidized.
- 17. (Original) A process according to claim 16 wherein the initiating compound is selected from methanol, hydrogen and dimethyl ether.
- 18. (Previously Presented) A process according to claim 1 wherein the mixture of the hydrocarbon and the oxygen-containing gas is fed to the catalyst when the catalyst has reached the temperature at which self-sustaining partial oxidation of the hydrocarbon will occur.
- 19. (Currently Amended) A process as claimed in claim 1 operated in combination with a catalysed water-gas shift reaction for the reduction of carbon monoxide in the hydrogen produced from the hydrogen hydrocarbon.
- 20. (Original) A process as claimed in claim 19 wherein the catalyst for the watergas shift reaction is a copper or iron based catalyst.

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21. (Previously Presented) A process according to claim 19 wherein the water-gas shift reaction catalyst is added to the rhodium based catalyst for the hydrogen generation reaction.

22. (Canceled)